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## INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

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<b>(21) International Application Number:</b> PCT/DK92/00060 <b>(22) International Filing Date:</b> 27 February 1992 (27.02.92) <b>(30) Priority data:</b> 0839/91 7 May 1991 (07.05.91) DK <b>(71) Applicant (for all designated States except US):</b> AGRO-FERM A/S [DK/DK]; Industrivej 11, DK-6870 Ølgod (DK). <b>(72) Inventors; and</b> <b>(75) Inventors/Applicants (for US only):</b> KJEL, Pauli [DK/DK]; Gl. Skolevej 47, DK-6731 Tjæreborg (DK). ANDERSEN, Margrethe [DK/DK]; Gl. Skolevej 47, DK-6731 Tjæreborg (DK). <b>(74) Agent:</b> HANSEN, Kaj; Rådgivende Ingeniørfirma, Elsegårde Skovvej 5, DK-8400 Ebeltøft (DK).		<b>(81) Designated States:</b> AT, AT (European patent), AU, BB, BE (European patent), BF (OAPI patent), BG, BJ (OAPI patent), BR, CA, CF (OAPI patent), CG (OAPI patent), CH, CH (European patent), CI (OAPI patent), CM (OAPI patent), DE, DE (European patent), DK, DK (European patent), ES, ES (European patent), FI, FR (European patent), GA (OAPI patent), GB, GB (European patent), GN (OAPI patent), GR (European patent), HU, IT (European patent), JP, KP, KR, LK, LU, LU (European patent), MC (European patent), MG, ML (OAPI patent), MR (OAPI patent), MW, NL, NL (European patent), NO, PL, RO, RU, SD, SE, SE (European patent), SN (OAPI patent), TD (OAPI patent), TG (OAPI patent), US.  <b>Published</b> <i>With international search report.</i> <i>With amended claims.</i>
<b>(54) Title:</b> METHOD FOR OBTAINING A CULTURE MEDIUM FROM PLANT SAP		
<b>(57) Abstract</b>  The procedure involves heat treatment of the plant juice, first in a temperature x time interval from 55 °C x 24 hours to 120 °C x 10 min., whereafter the plant juice is cooled to 50 °C - 60 °C and the pH value is set at 7.5 - 8.5 by addition of a base. Hereafter the plant juice is converted by enzymic hydrolysis by means of proteolytic enzymes such as proteases and peptidases, while keeping the pH value constant at 7.5 - 8.5 by continuous addition of base until the hydrolysis is over. By the procedure a medium is formed which is well suited as a nutritive substrate for vitamin and amino acid demanding micro-organisms, which form organic acids or amino acids. By the procedure it is possible in a cheap and simple manner to convert plant juice to organic acids or amino acids.		

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## METHOD FOR OBTAINING A CULTURE MEDIUM FROM PLANT SAP

## DESCRIPTION

The present invention relates to a procedure for conversion of plant juice to a medium which is well suited as a nutritive medium for micro-organisms requiring vitamin and amino acids, for example bacteria which form organic acids or amino acids.

In connection with agro-industrial productions, for example production of potato starch and vegetable pellets, there will be a residual product in the shape of a liquid or juice, which hitherto has been sprayed as manure on fields.

The juice has a content of dry matter of 2%-6%. This dry matter contains among other things fibres, protein, carbohydrates, vitamins and free amino acids.

15 This juice thus contains all the substances which are necessary to promote growth of the most demanding micro-organisms.

However, the juice can only be used as substrates for micro-organisms which do not make heavy demands on the content of free amino acids, or which are capable of forming proteolytic exoenzymes, e.g. bacillus species.

Thus, bacteria of the family Lactobacillus and auxotrophic mutants which have specific amino-acid demands, e.g. mutants of Corynebacterium glutamicum and Brevibacterium lactofermentum, which are used for the production of amino acids, e.g. glutamic acid, L-lysine and threonine, cannot spontaneously utilize the plant juice because most amino acids are bonded in the proteins.

This fermentation process is slow and therefore not applicable in practice.

It is well known that it is possible to hydrolyse protein to free amino acids either by acid hydrolysis by

using strong acids and high temperatures or by enzymic hydrolysis using protease and peptidase.

However, it is not possible to carry out acid hydrolysis on an aqueous solution of protein of so low a concentration as the liquid in question.

Nor will it be possible to use enzymic hydrolysis, as it will be necessary to use very large quantities of enzymes so that the process will be too expensive and therefore economically forbidding.

10 It is the purpose of the present invention to describe a procedure by which the plant juice can be converted into a medium which is well suited as a nutritive substrate to culture e.g. *Lactobacillus delbruckii*, *Lactobacillus plantarum* and amino-acid demanding mutants of *Brevibacterium*  
15 *lactofermentum* and *Corynebacterium glutamicum*.

This procedure makes it possible to utilize the plant juice in an industrial fermentation process in the production of e.g. lactic acid or amino acids, which both are products which find extensive application in the food and feedstuffs  
20 industries and the chemical industry.

This is achieved by the described procedure in the characterizing part of claim 1.

By the said procedure it is also possible as described in claim 2 to use enzymes occurring naturally in some plant  
25 juices.

Claim 3 deals with a procedure for production of enzymes to be used in the hydrolysis, and

Claim 4 deals with enzymic treatment of the plant juice with commercial enzymes, e.g. *ALCALASE*<sup>®</sup>.

30 The following examples serve to illustrate the invention.

EXAMPLE 1

In the production of v g tabl pellets the cut grass or alfalfa is pressed at once, thereby producing vegetable juice, or it is heated first and then pressed, whereby 5 brown juice is produced.

The brown juice contains 2-5% dry matter of which 15-35% is protein, abt. 22% ashes, and 20-40% is carbohydrate.

In this case a vacuum evaporated brown juice concentrate has been produced.

10 This concentrated brown juice contains 22% dry matter of which 5% is protein.

The concentrated brown juice is heated to 80°C for ten hours in order to pasteurize the brown juice.

The temperature is set at 55°C, pH is set at 8.0 with 15 6N ammonia, whereafter the temperature is held at 55°C and the pH at 8.0 (pH-Stat) with current adjustment of the pH by addition of 6N ammonia.

The hydrolysalation is stopped when the consumption of base corresponds to a degree of hydrolysis (DH) of a minimum of 20 80%.

The degree of hydrolysis is calculated as follows:

$$DH = B \cdot \frac{1}{6} \cdot \frac{N_B}{MP} \cdot \frac{1}{h_{tot}} \cdot 100\%, \text{ where}$$

B: Consumption of base in litres.

1

—: Calibration factor for pH-Stat, at pH=8 is used  
6 the value 1.0.

25  $N_B$ : Normality of base.

MP: Protein mass in kg.

$h_{tot}$ : Total number of peptide bonds. Here  $h_{tot}=8.0$  is used.

In this example 122 ml 6N ammonia is consumed after 24 hours for hydrolysis of 2 l concentrated brown juice, corresponding to a degree of hydrolysis of 91.5%.

The hydrolysis process is stopped.

- 5 The hydrolyzed concentrated brown juice is now used in a culture medium to culture *Corynebacterium glutamicum* ATCC 21526, a strain demanding homoserine and leucine.

The culture medium is composed as follows:

10% molassis (calculated as glucose).

- 10 20% concentrated hydrolyzed brown juice, corresponding to 1% protein hydrolysate.

0.07%  $\text{KH}_2\text{PO}_4$

0.05%  $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$

0.3% urea

- 15 0.5%  $(\text{NH}_4)_2\text{SO}_4$

3%  $\text{CaCO}_3$

pH set at 7.5.

Culture is carried out at 30°C for 4 x 24 hours in a 1-litre fermentor with aeration.

- 20 Culture in this nutritive medium produces 22.5 mg/ml of L-lysine.

Culture in a substrate with non-hydrolyzed brown juice produces only 4.3 mg/ml of L-lysine.

In a medium where the brown juice is substituted by soya bean cake sulphuric acid decomposate there is a production of 19.5 mg/ml of L-lysine.

#### EXAMPLE 2

5 Potato fruit juice is one of the residual products in the production of starch.

Potato fruit juice contains the parts of the potato which in the process of leaching out of the starch have decomposed, including part of the nitrogenous compounds, protein, amino  
10 acids, etc.

The potato fruit juice used in the example contains 4.4% dry matter of which 2.0% is protein ( $N \times 6.25$ ).

The potato fruit juice is heat treated at 120°C for 20 min.

The heat treated potato fruit juice is cooled to 55°C,  
15 pH is set at 8.0 with 4N ammonia, whereafter 0.01% ALCALASE<sup>R</sup> 2.4L is added.

pH is kept constant at 8.0 (pH-Stat) by adding 4N ammonia or 4N sodium hydroxide.

After 4 hours a degree of hydrolysis (DH) of 35% is obtained.

20 The hydrolyzed potato fruit juice is ultrafiltrated so that particles and molecules with a molecular weight higher than 10,000 are removed.

The ultrafiltrate contains partially hydrolyzed protein and free amino acids.

25 The ultrafiltrate is added 2% glucose, pH is set at 7.0, it is autoclaved at 110°C for 15 min. and used as a culture medium for various bacteria. After incubation at 37°C for 24 hours the following growth is obtained, measured as optical density at 450nm ( $OD_{450}$ ).

30 In the case of culture of potato fruit juice ultrafiltrate which is not

subjected to enzymic treatment the growth will in most cases be smaller.

TABLE:

		Enzyme treated	Not enzyme treated
5	Bacteria		
	<i>Corynebacterium glutamicum</i> ATCC 21526	6.6	0.5
	<i>Brevibacterium lactofermentum</i> ATCC 21798	4.4	1.2
	<i>Brevibacterium lactofermentum</i> ATCC 13869	6.5	1.8
	<i>Bacillus subtilis</i> ATCC 6051	1.9	2.0
10	<i>Lactobacillus casei</i> ATCC 11443	2.5	0.5
	<i>Lactobacillus bulgaricus</i> Chr.Hansen's Lab	1.5	0.3

EXAMPLE 3

In the culture of *Bacillus amyloliquefaciens* ATCC 23842 in a sterile medium consisting of brown juice with a content of protein of 1% it is possible to produce proteolytic enzymes which can be used in a subsequent hydrolysis of plant juice.

After culture at 37°C for 24 hours under aeration an enzyme activity is obtained in the brown juice of  $2.5 \times 10^{-2}$  Anson units/ml, which corresponds to the enzyme activity used when using commercial enzymes such as e.g. ALCALASE<sup>®</sup> 0.6L.



## P A T E N T   C L A I M S

1. Procedure for the conversion of plant juice to a medium which is well suited as a nutritive substrate for micro-organisms demanding vitamins and amino acids, e.g. bacteria,  
5 which form organic acids or amino acids, c h a r a c t e -  
r i z e d by the plant juice first being heat treated in a temperature x time interval from 55°C x 24 hours to 120°C  
10 min., depending on the nature of the plant juice, and by the subsequent cooling of the plant juice to 50°C, and  
10 by the pH value being set at 7.5 - 8.5 by addition of a base, preferably ammonia, whereafter the plant juice is converted by enzymic hydrolysis by means of proteolytic enzymes, preferably protease and peptidase under continuous stirring and by the pH value being kept constant at 7.5-8.5  
15 under continued addition of ammonia until the hydrolysis proces is over.
2. Procedure for the conversion of plant juice according to claim 1, c h a r a c t e r i z e d by the fact that the enzymes are proteolytic enzymes occurring naturally  
20 in some plant juices, e.g. grass juice.
3. Procedure for the conversion of plant juice according to claim 1, c h a r a c t e r i z e d by the fact that the enzymes are proteolytic enzymes formed by micro-organisms cultured in the plant juice or in a nutritive  
25 substrate of a kind other than the plant juice which is to be converted.
4. Procedure for the conversion of plant juice according to claim 1, c h a r a c t e r i z e d by the fact that th plant juice is enzym -treated by addition of a proteo-  
30 lytic enzyme, e.g. ALCALASE<sup>R</sup>.

## AMENDED CLAIMS

[received by the International Bureau on 12 October 1992(12.10.92);  
original claims 1,3 and 4 amended; claim 2 unchanged  
(1 page)]

1. Procedure for the conversion of plant juice to a medium  
which is well suited as a nutritive substrate for bacteria  
demanding vitamins and amino acids, which form organic  
acids or amino acids, c h a r a c t e r i z e d by the  
5 plant juice first being heat treated in an interval for re-  
lated values of temperature and time, ranging from 55°C and  
24 hours to 120°C and 10 minutes, depending on the nature  
of the plant juice, and by the subsequent cooling of the  
plant juice to 50°C - 60°C, and by the pH value being set  
10 at 7.5 - 8.5 by addition of a base, preferably ammonia,  
whereafter the plant juice is converted by enzymic hydro-  
lysis by means of proteolytic enzymes, preferably proteases  
and peptidases under continuous agitation and by the pH  
value being kept constant at 7.5-8.5 under continued addi-  
15 tion of a base until the hydrolysis process is over.

2. Procedure for the conversion of plant juice according  
to claim 1, c h a r a c t e r i z e d by the fact that  
the enzymes are proteolytic enzymes occurring naturally  
in some plant juices, e.g. in grass juice.

20 3. Procedure for the conversion of plant juice according  
to claim 1, c h a r a c t e r i z e d by the fact that the  
enzymes are proteolytic enzymes formed by micro-organisms  
cultivated in the plant juice or formed by the cultivation  
of micro-organisms in a nutritive substrate of a kind other  
25 than the plant juice which is to be converted.

4. Procedure for the conversion of plant juice according  
to claim 1, c h a r a c t e r i z e d by the fact that  
the plant juice is hydrolyzed by addition of a proteolytic  
enzyme, e.g. ALCALASE (®).

# INTERNATIONAL SEARCH REPORT

International Application No PCT/DK 92/00060

<b>I. CLASSIFICATION OF SUBJECT MATTER</b> (If several classification symbols apply, indicate all) <sup>6</sup>		
According to International Patent Classification (IPC) or to both National Classification and IPC		
IPC5: C 12 N 1/00, 1/20		
<b>II. FIELDS SEARCHED</b>		
Minimum Documentation Searched <sup>7</sup>		
Classification System	Classification Symbols	
IPC5	C 12 N	
Documentation Searched other than Minimum Documentation to the Extent that such Documents are Included in Fields Searched <sup>8</sup>		
SE,DK,FI,NO classes as above		
<b>III. DOCUMENTS CONSIDERED TO BE RELEVANT<sup>9</sup></b>		
Category <sup>*</sup>	Citation of Document, <sup>11</sup> with indication, where appropriate, of the relevant passages <sup>12</sup>	Relevant to Claim No. <sup>13</sup>
A	FR, A, 904488 (NEUERBURG & PANKOFER KOMMANDIT-GESELLSCHAFT) 20 May 1944, see the whole document --	1
A	CH, A, 523963 (SICALY) 31 July 1972, see the whole document --	1
A	GB, A, 2090288 (ROQUETTE FRERES S.A.) 7 July 1982, see the whole document --	1
A	EP, A3, 0065246 (ELKAWI AG) 24 November 1982, see page 4, line 20 - page 5, line 12 -- -----	1
<p><b>* Special categories of cited documents:</b><sup>10</sup></p> <p>"A" document defining the general state of the art which is not considered to be of particular relevance</p> <p>"E" earlier document but published on or after the international filing date</p> <p>"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)</p> <p>"O" document referring to an oral disclosure, use, exhibition or other means</p> <p>"P" document published prior to the international filing date but later than the priority date claimed</p> <p>"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention</p> <p>"X" document of particular relevance, the claimed invention cannot be considered novel or cannot be considered to involve an inventive step</p> <p>"Y" document of particular relevance, the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.</p> <p>"&amp;" document member of the same patent family</p>		
<b>IV. CERTIFICATION</b>		
Date of the Actual Completion of the International Search	Date of Mailing of this International Search Report	
6th August 1992	1992 -08- 12	
International Searching Authority	Signature of Authorized Officer	
SWEDISH PATENT OFFICE	Mikael G:sonBergstrand	

**ANNEX TO THE INTERNATIONAL SEARCH REPORT  
ON INTERNATIONAL PATENT APPLICATION NO.PCT/DK 92/00060**

This annex lists the patent family members relating to the patent documents cited in the above-mentioned international search report.  
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Patent document cited in search report	Publication date	Patent family member(s)	Publication date
FR-A- 904488	44-05-20	NONE	
CH-A- 523963	72-07-31	DE-A- 2022359 FR-A- 2044072	70-11-19 71-02-19
GB-A- 2090288	82-07-07	DE-A-C- 3150336 FR-A-B- 2496689 NL-A- 8105721 US-A- 4766070	82-07-22 82-06-25 82-07-16 88-08-23
EP-A3- 0065246	82-11-24	CA-A- 1179957 CH-A-B- 651063 JP-A- 57192316	84-12-25 85-08-30 82-11-26